

Refrigeration Control for Operating Cost Reduction

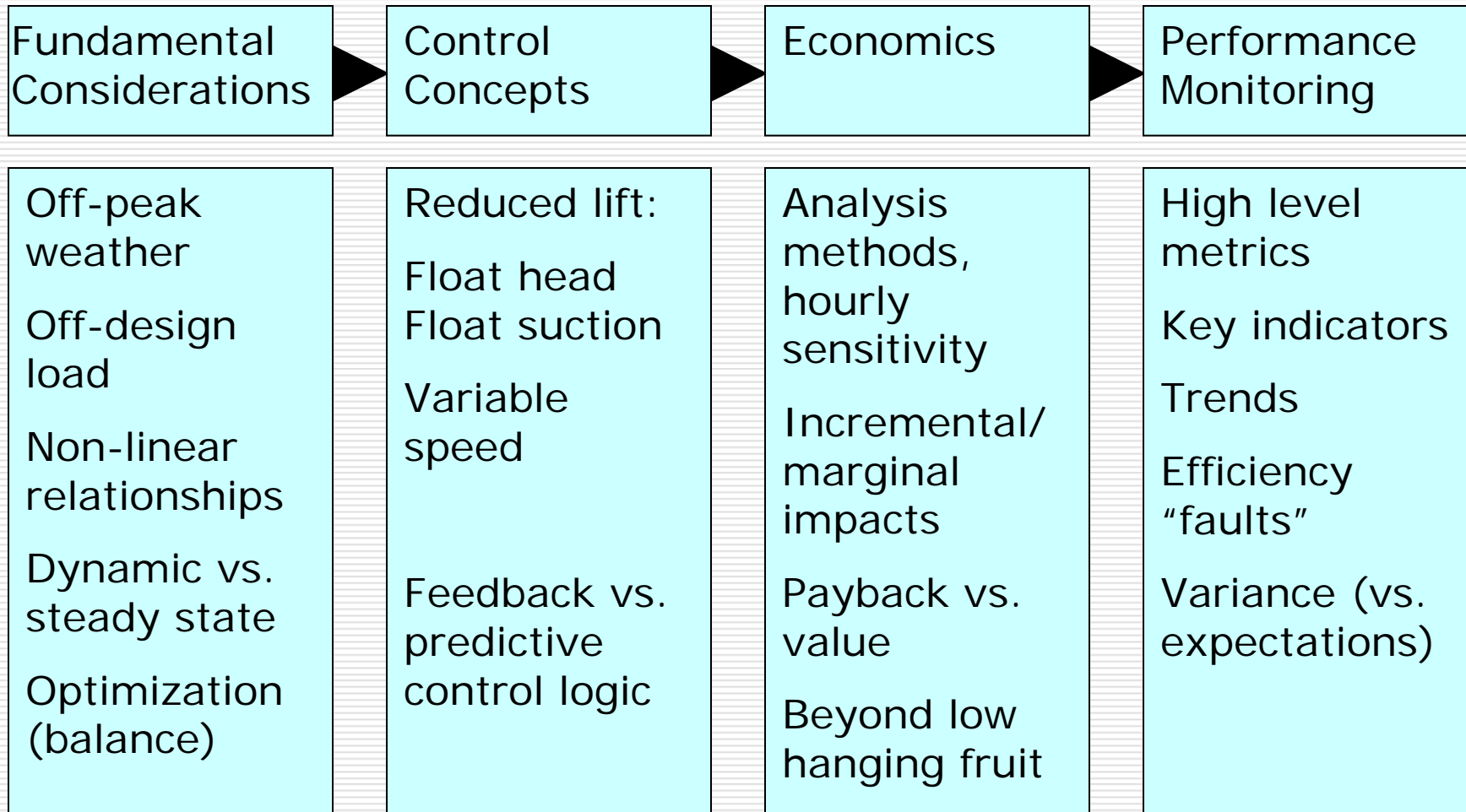
ASHRAE 2007 Annual Meeting
Long Beach, California

Doug Scott
VaCom Technologies

Topics

- Fundamentals
- Control Strategies
- Economics & Case Studies
- Maintaining Performance

Concept flow



Basic considerations

- Comparing design vs. hourly operation:
 - Actual hourly load vs. peak design load
 - Actual hourly weather vs. peak ambient
 - dynamic operation vs. steady state
 - Non-linear energy relationships
- Concepts relating refrigeration systems to energy use:
 - Vapor compression cycle
 - Temperature “lift”
 - Variable speed and “affinity” laws

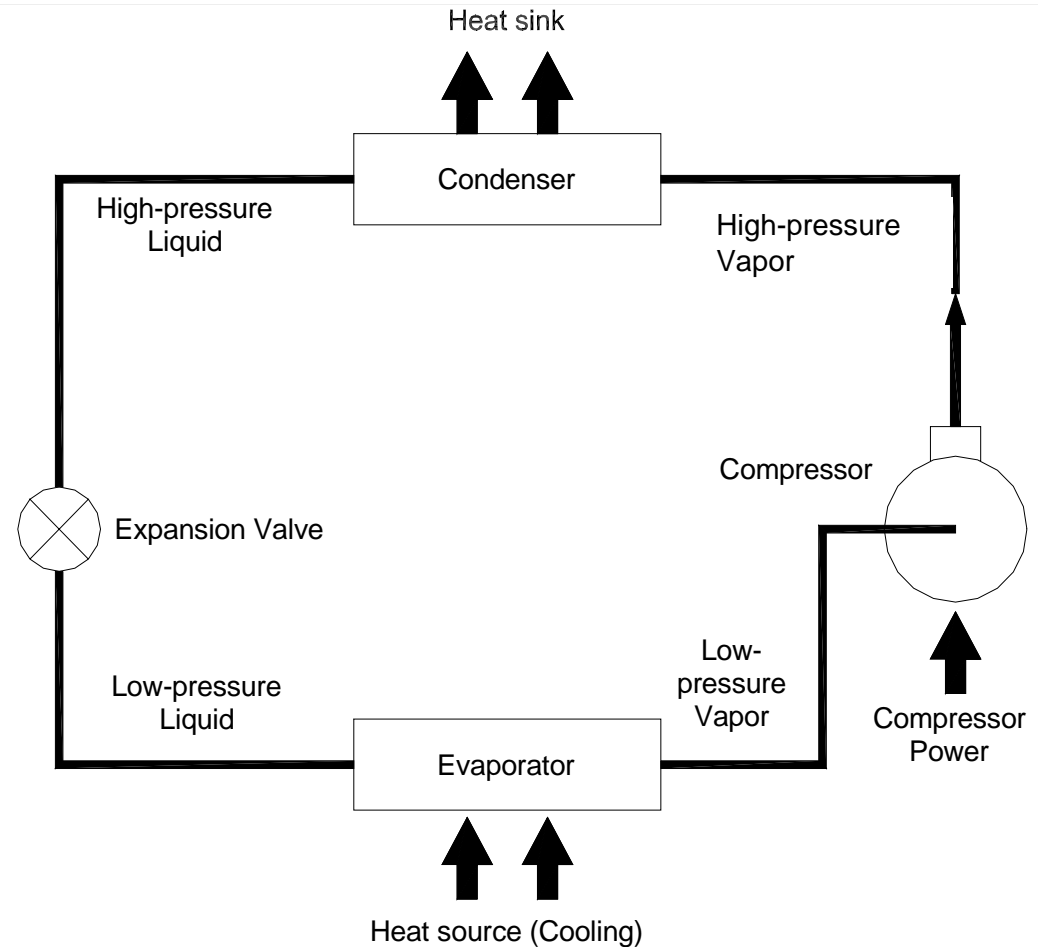
General opportunities

- Minimize lift
 - Float head pressure
 - Float suction
- Maximize refrigerant performance
 - Separate mass flow and enthalpy
- Condenser / evaporator performance
 - Utilize all surface all the time
 - Use inherent advantage of variable speed
- Ongoing maintenance opportunities
- Monitor performance

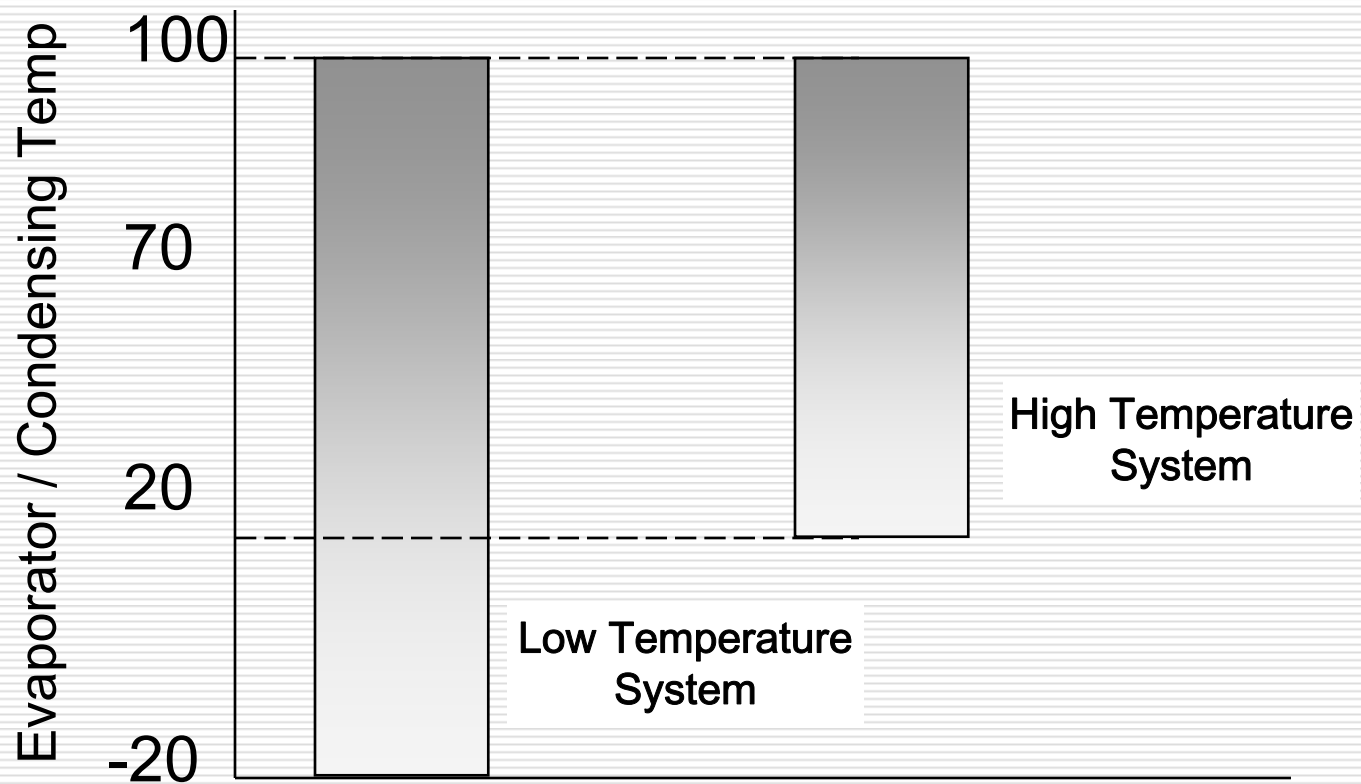
Vapor compression cycle

BASIC CONCEPTS

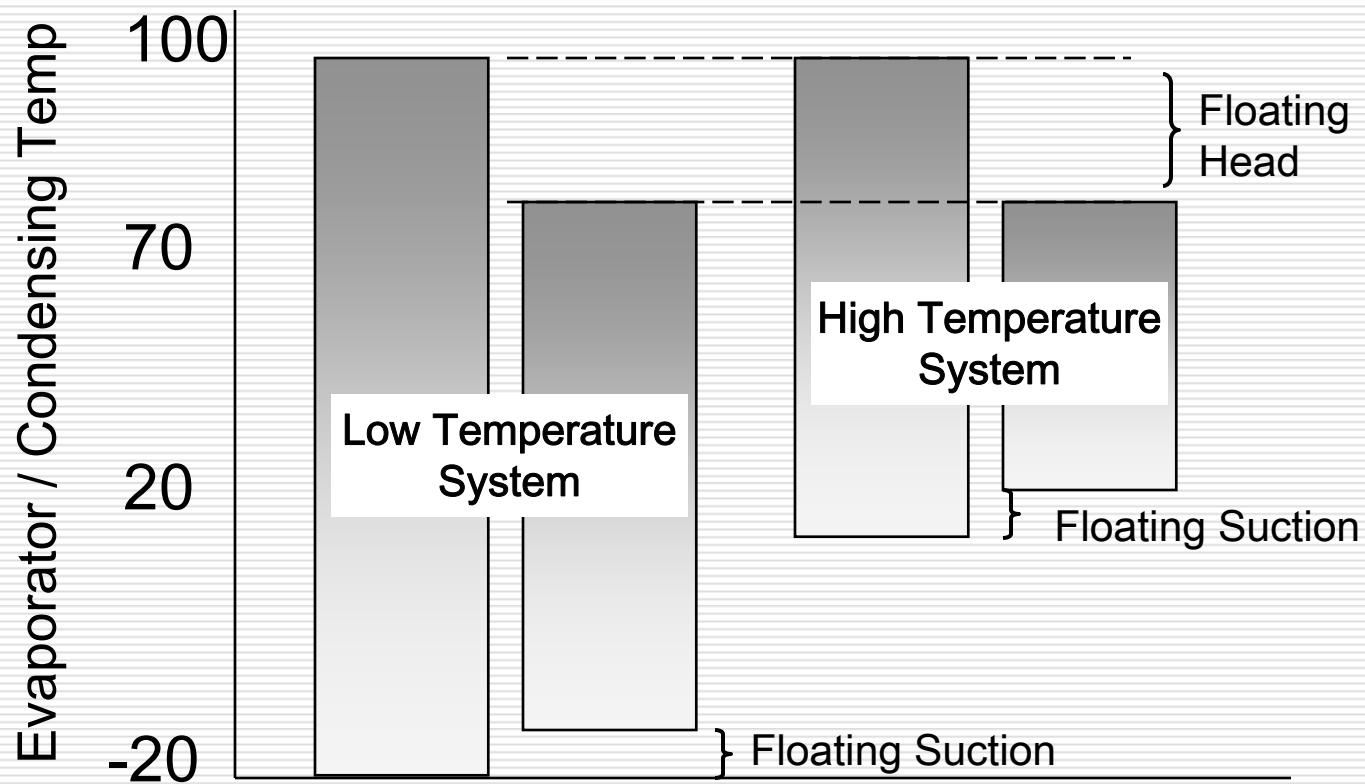
- ❑ Refrigeration moves heat rather than creating cold
- ❑ Energy is conserved – energy in equals energy out
- ❑ Compressor pumps vapor; the refrigerant creates the cooling effect



Cooling system "lift"



Reduced lift at non-peak, part load



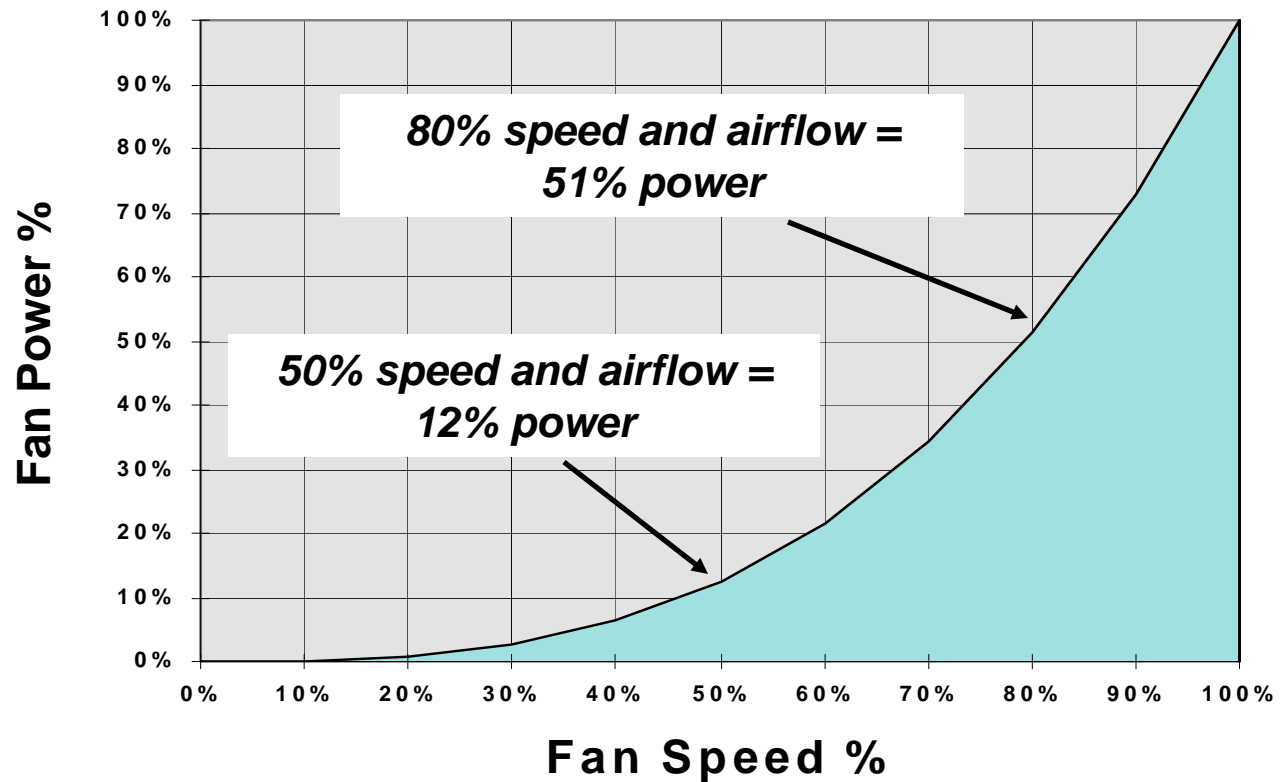
Variable speed fan control

Third power relationship ("affinity" laws)

Airflow varies directly with change in speed

Air pressure drop varies with the square of change in speed

Fan power varies with cube of change in speed



Heat Rejection

Heat rejection improvement

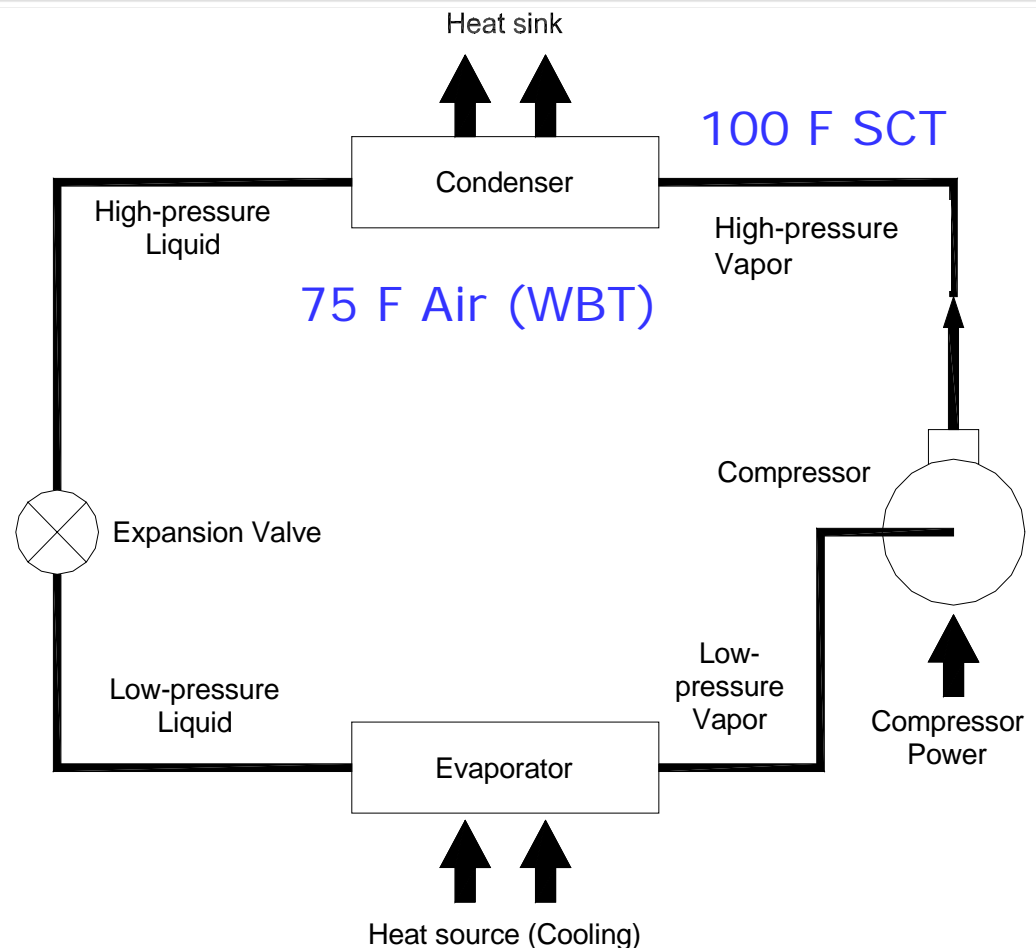
- Why start here?
 - All heat/energy leaves through condenser
 - Largest single savings opportunity on most systems
- Condenser sizing
 - Bigger is better, but bigger means more fan power
 - Goal: balance between size and power (and cost)
- Size shown by TD (temperature difference)
 - $TD = \text{condensing temperature} - \text{ambient temperature}$
 - Smaller TD = larger condenser
- Floating head pressure control strategies:
 - How low, how fan is controlled, how setpoint is set

Evap condenser TD example

Historical design:
75 F entering WBT +
25 F TD =
100 F condensing

Larger condenser:
75 F entering WBT +
14 F TD =
89 F condensing

= Lower Lift (by 11 F)

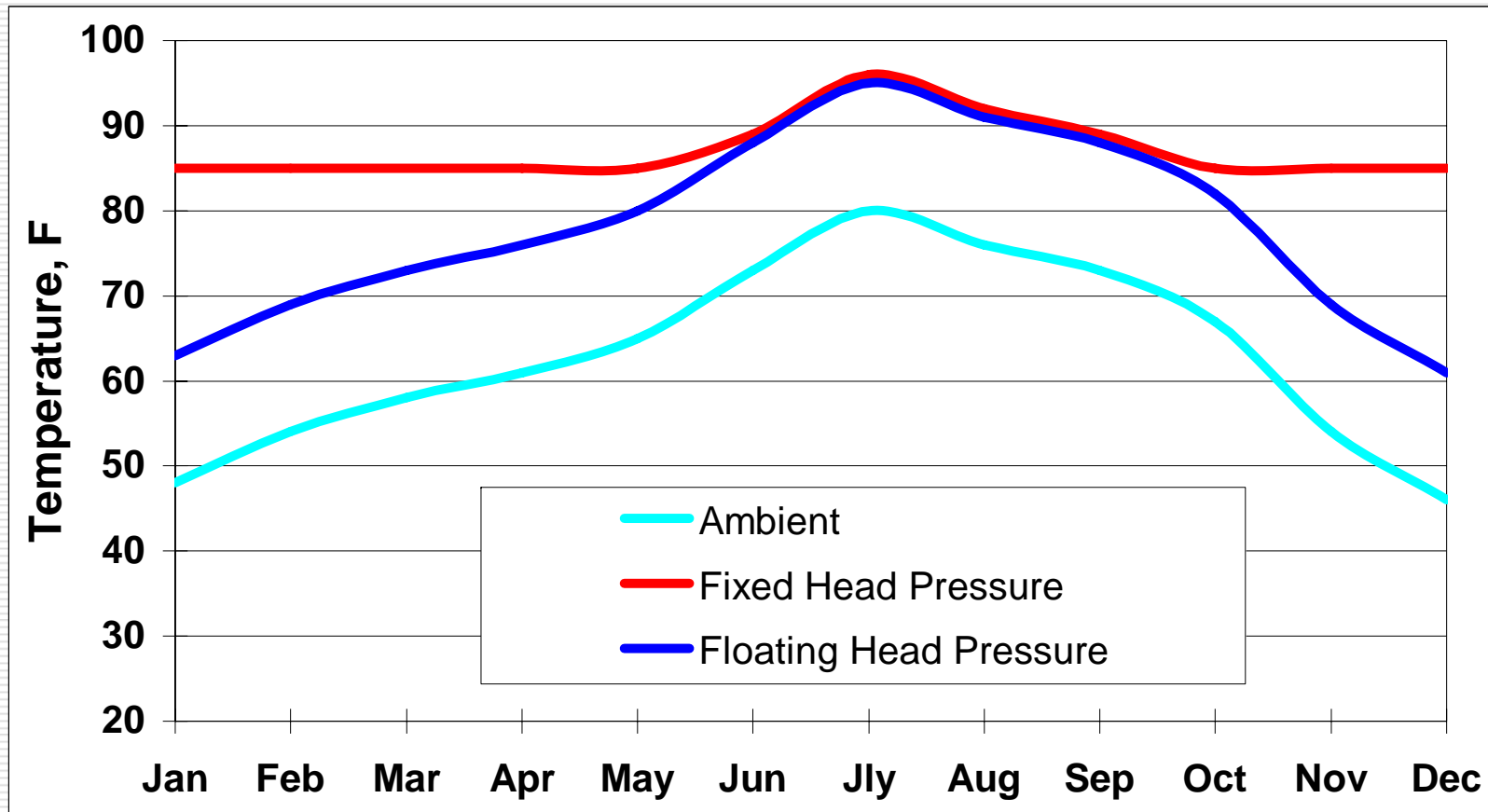


Specific efficiency example

Size	Motors	Capacity (10 F)	kW	BTUH/ Watt	% Difference
50	2 -- 5 HP	400	8.9	44.9	
52	3 -- 1.5 HP	450	4.0	112.3	150%

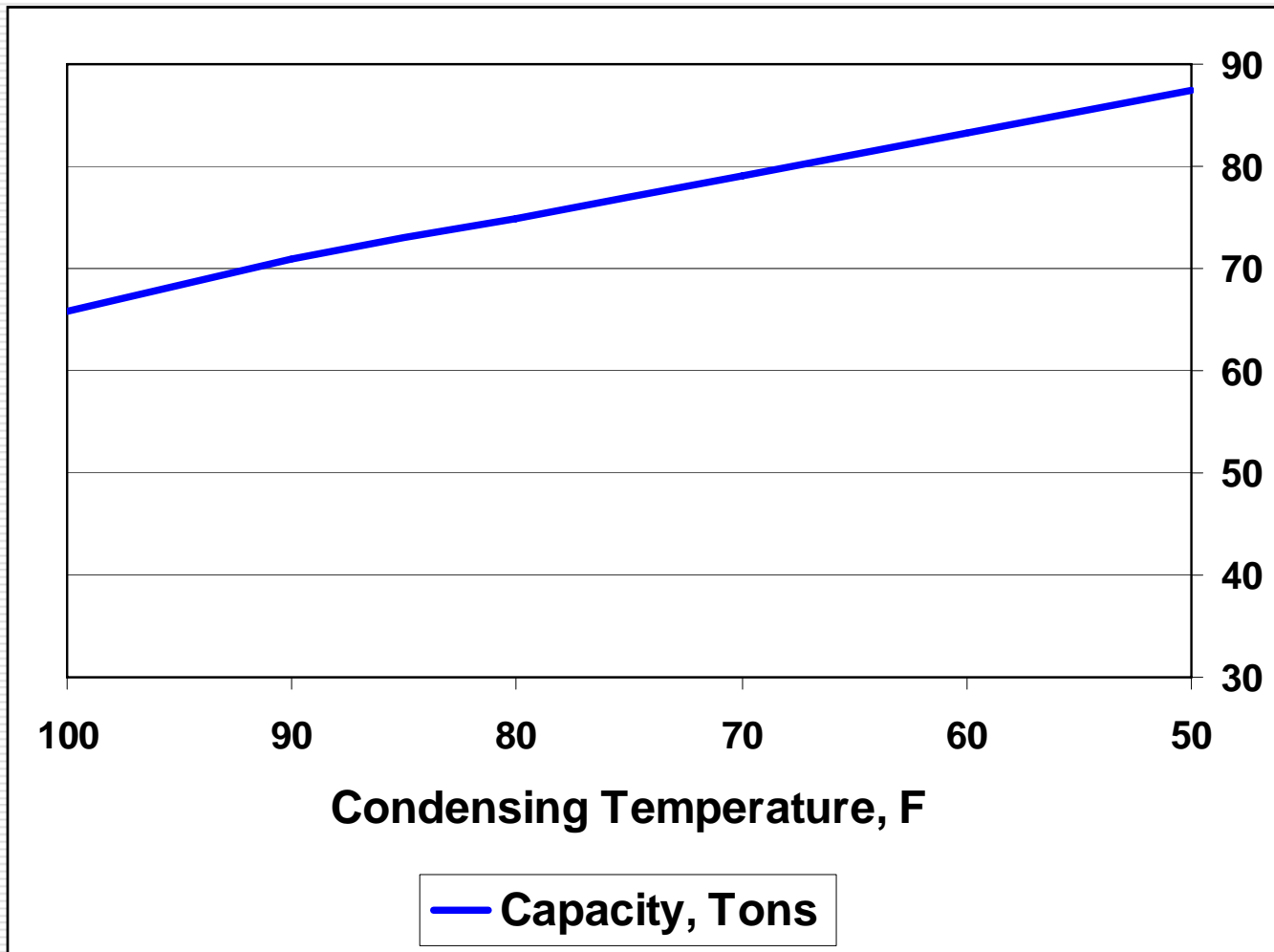
- ❑ Example of two consecutive air cooled condenser models from one manufacturer.
- ❑ Air velocity and fan motor size is used to achieve a large range of catalog sizes, first cost and footprint, some models are energy "hogs".

Fixed vs. floating head pressure (floating condensing temperature)



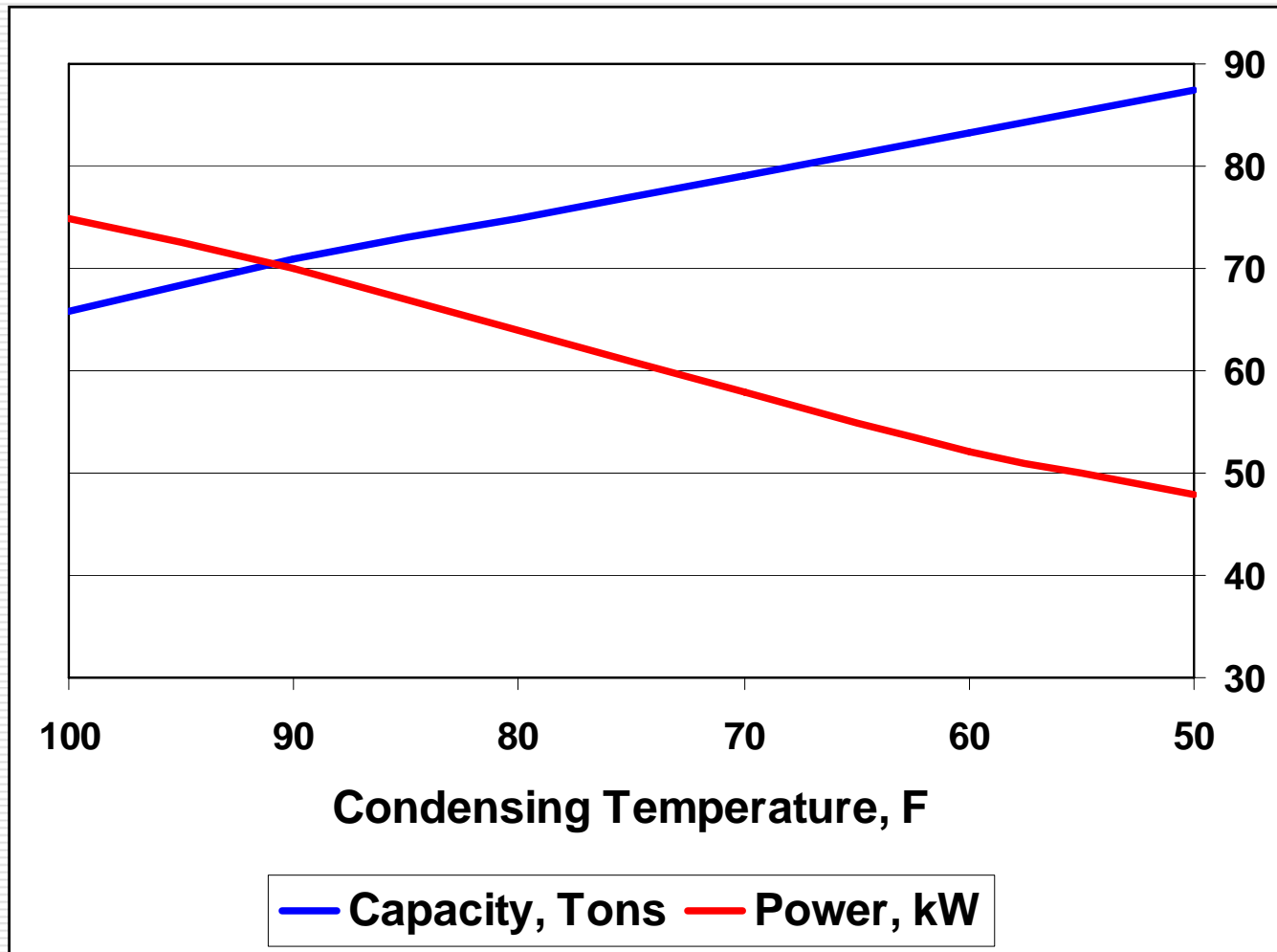
Floating head pressure

Impact on cooling capacity



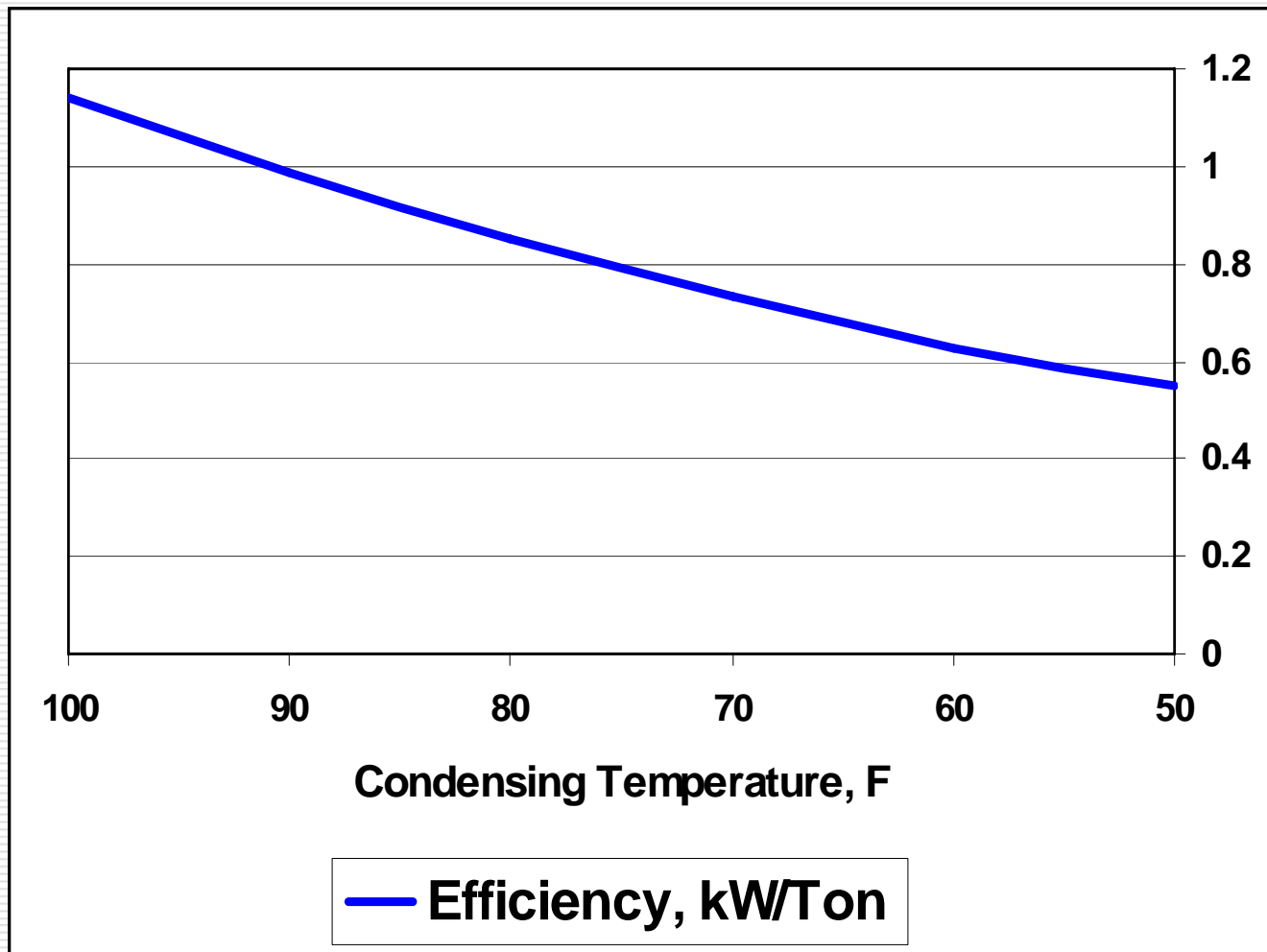
Floating head pressure

Impact on capacity and power



Floating head pressure

Net effect on efficiency



Floating head pressure

Compressor efficiency examples

Medium Temperature (+20 F)				
SCT (F)	Capacity	Power	EER (Btu/Watt)	Increase vs 100 SCT
100	79	7.5	10.5	0%
90	85	7	12.1	15%
80	90	6.4	14.1	34%
70	95	5.8	16.4	55%
60	100	5.2	19.2	83%
50	105	4.8	21.9	108%

Low Temperature (-25 F)				
SCT (F)	Capacity	Power	EER (Btu/Watt)	Increase vs 100 SCT
100	48	8.4	5.7	0%
90	52	8.1	6.4	12%
80	55	7.7	7.1	25%
70	58	7.2	8.1	41%
60	61	6.8	9.0	57%
50	64	6.5	9.8	72%

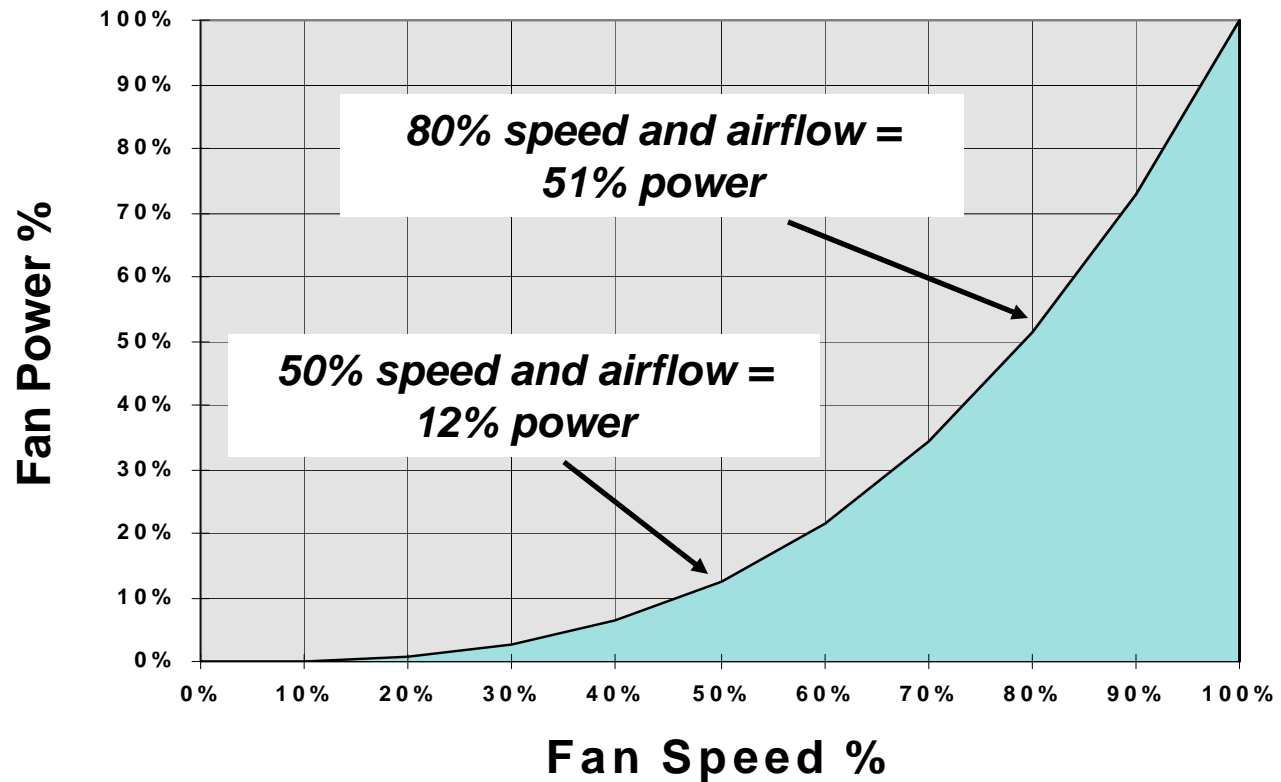
Variable speed fan control (again)

Third power relationship ("affinity" laws)

Airflow varies directly with change in speed

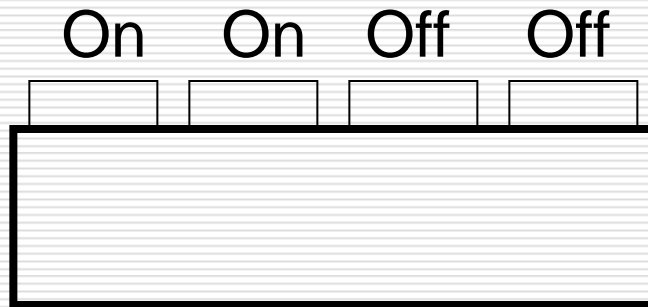
Air pressure drop varies with the square of change in speed

Fan power varies with cube of change in speed

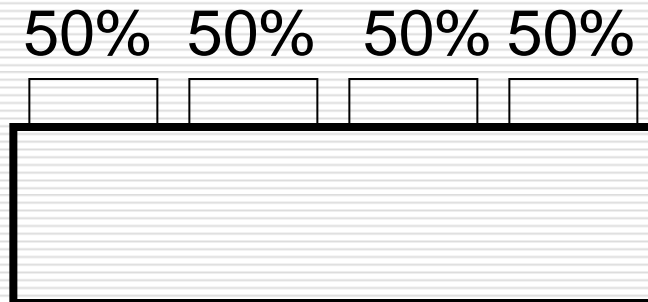


Part load performance

Variable speed vs. fan cycling



50% capacity
50% power
80 BTUH/Watt

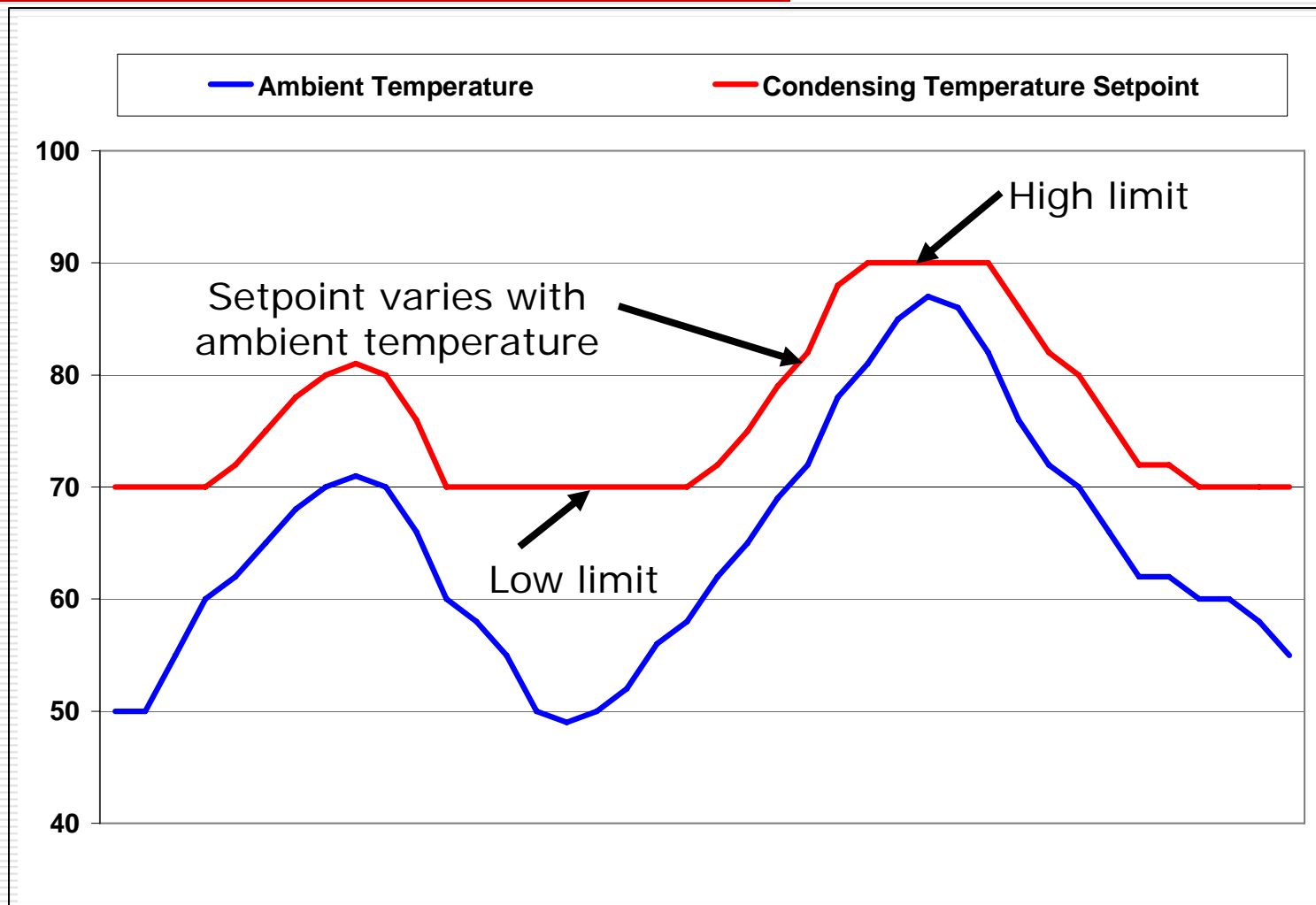


50% capacity
12% power
330 BTUH/Watt

Part load efficiency increased by 300% with variable speed

Floating head pressure

Variable setpoint control



Floating head pressure

Energy savings potential

Energy savings result from:

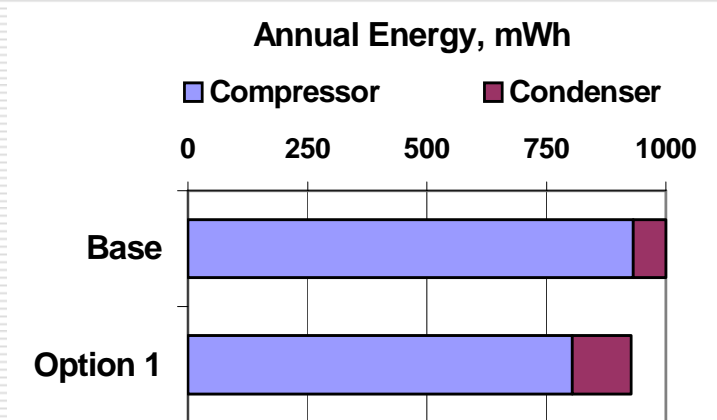
- ❑ Lower head pressure at compressor (and lower condensing temperature at condenser)
- ❑ Lower fan power
 - Variable speed
 - Variable setpoint
- ❑ Overall optimum system balance
 - Minimum total fan power + compressor power
- ❑ Savings with optimum FHP
 - 12-20% of annual compressor and condenser energy
 - *But, can be zero without proper control strategy*

FHP case study

- ❑ Cold storage warehouse in Stockton, California
- ❑ Evaporative condenser (average efficiency)
- ❑ Hourly simulation analysis
- ❑ Base case = fixed setpoint at 85 F SCT
- ❑ Analysis options
 - Float SCT using fixed setpoint
 - Add variable setpoint
 - Add variable speed with fixed setpoint
 - Add variable speed with variable setpoint

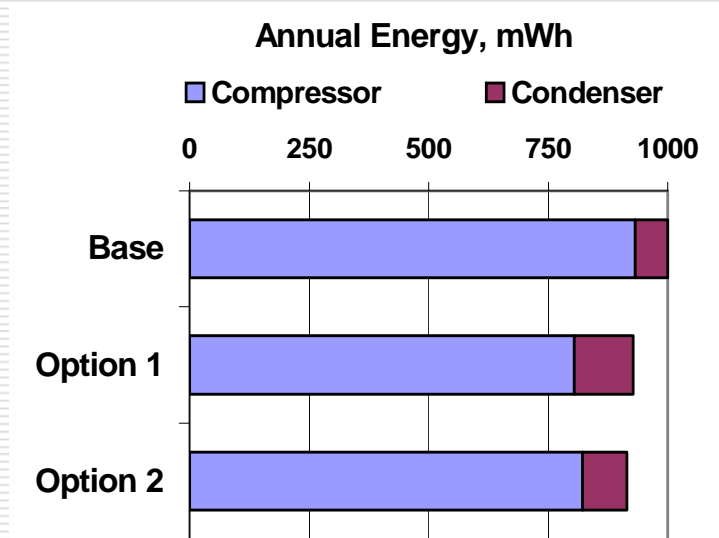
- ❑ Results show importance of control strategy

Results – fixed setpoint



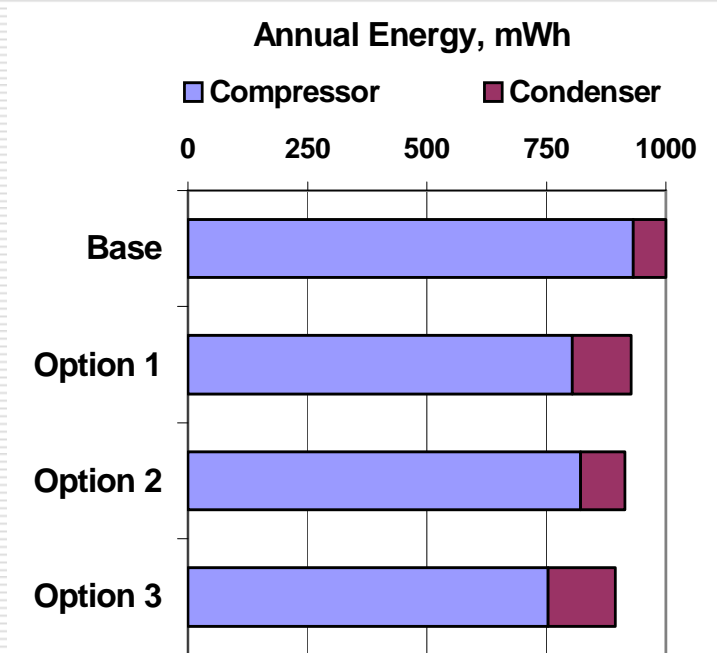
Control Options				Savings	Payback	NPV
FHP	FSP	VSP	VFD			
X	X			\$ 6,400	0.3	\$ 63,500

Results – variable setpoint



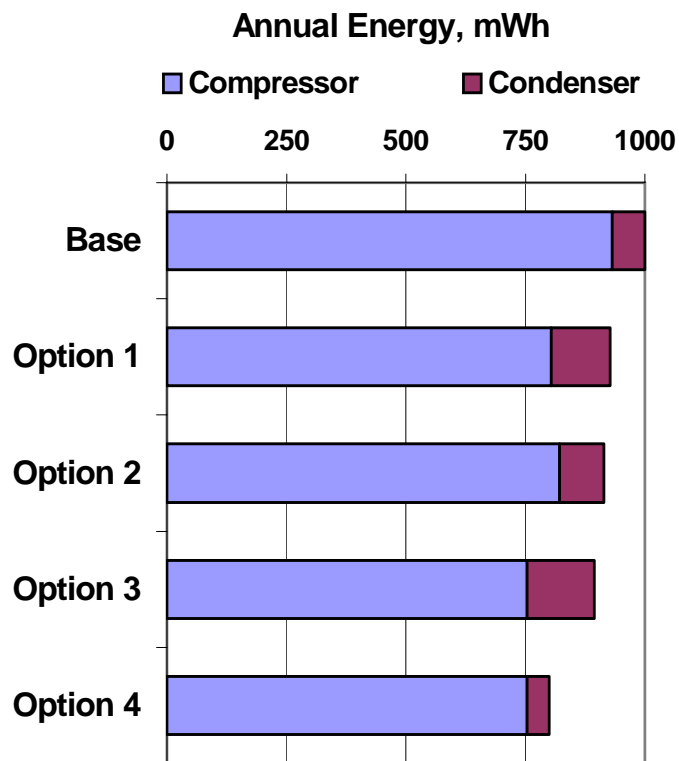
Control Options				Savings	Payback	NPV
FHP	FSP	VSP	VFD			
X	X			\$ 6,400	0.3	\$ 63,500
X		X		\$ 8,400	0.6	\$ 80,300

Results – fixed SP, variable speed



	Control Options				Savings	Payback	NPV
	FHP	FSP	VSP	VFD			
Base							
Option 1	X	X			\$ 6,400	0.3	\$ 63,500
Option 2	X		X		\$ 8,400	0.6	\$ 80,300
Option 3	X	X		X	\$ 9,100	4.4	\$ 52,900

Results – variable SP & speed

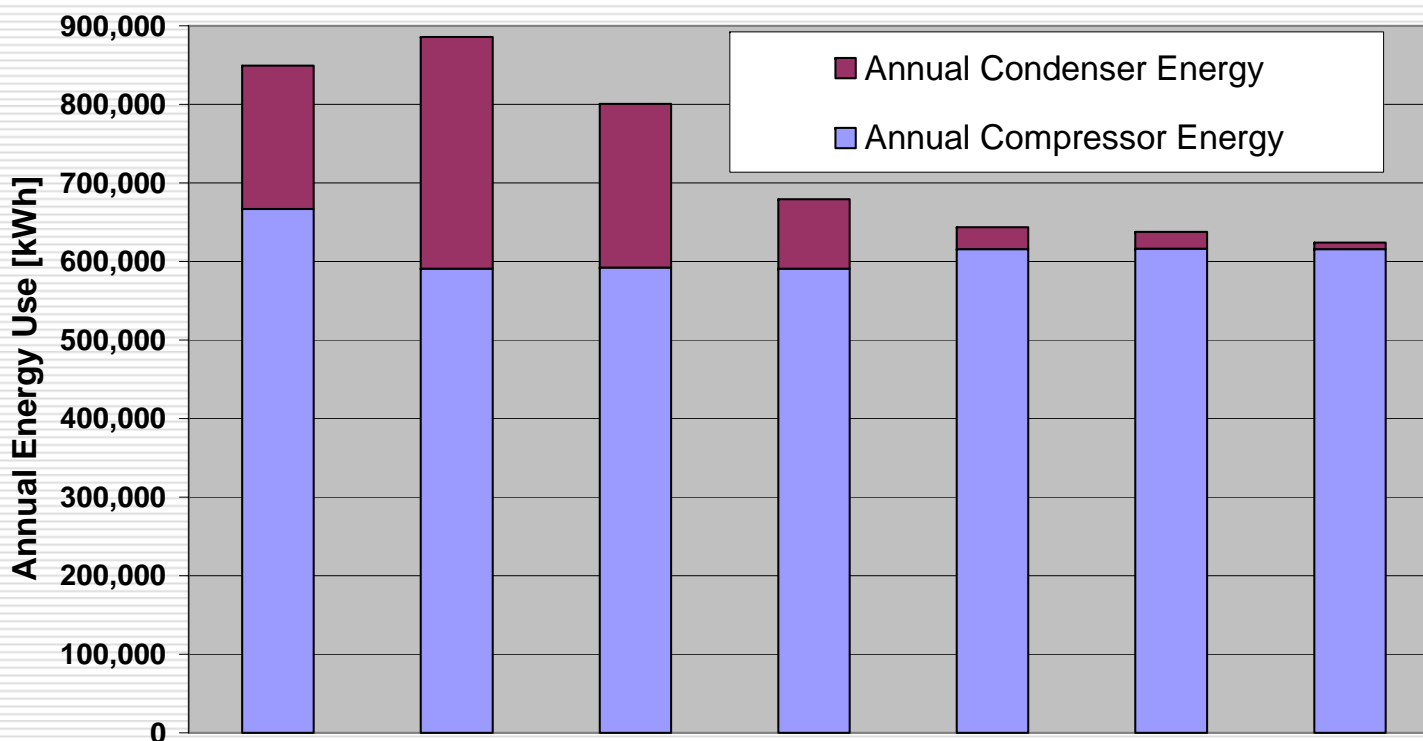


Control Options	FHP	FSP	VSP	VFD	Savings	Payback	NPV
	X	X			\$ 6,400	0.3	\$ 63,500
	X		X		\$ 8,400	0.6	\$ 80,300
	X	X		X	\$ 9,100	4.4	\$ 52,900
	X		X	X	\$ 21,600	2.1	\$ 175,300

Supermarket condenser study

- ❑ Fort Worth TX weather, full size supermarket
- ❑ Hourly simulation (DOE2.2R)
- ❑ Comparison of condenser fan power
 - Standard (typical 1.5 HP 1140 RPM)
 - Mid-range (lower power and speed)
 - Very low power (1/2 HP motors 800 RPM or lower)
- ❑ Comparison of fan control
 - Fan cycling
 - Variable speed (assuming use of inverters for cost)
- ❑ Comparison of setpoint methods
 - Fixed setpoint
 - Variable setpoint (DBT plus TD)

Supermarket condenser study



Condenser Fan Power	Standard	Standard	Mid-Range	Very Low	Standard	Mid-Range	Very Low
Floating Head	No	Yes	Yes	Yes	Yes	Yes	Yes
Fan Control	Cycling	Cycling	Cycling	Cycling	Variable	Variable	Variable
Setpoint Control	Fixed	Fixed	Fixed	Fixed	Variable	Variable	Variable
Payback, Years		N/A	0.9	2.3	0.9	1.1	2.4
Incremental Payback				2.9		8.1	24.0

Note about variable setpoint

- *Variable setpoint or ambient following setpoint control is not the only means of optimizing the balance between condenser and compressor power. Other methods may be superior and ultimately displace ambient following control.*

Variable Volume Air Unit Control

Variable volume air unit control

- ❑ Vary fan speed in freezers and coolers as primary means of temperature control
- ❑ Strategy: reduce speed to 60-70%, then float suction up or cycle off cooling valve
- ❑ Third power rule applies to fan power
- ❑ Saving from:
 - Reduced fan energy
 - Reduced refrigeration cooling load

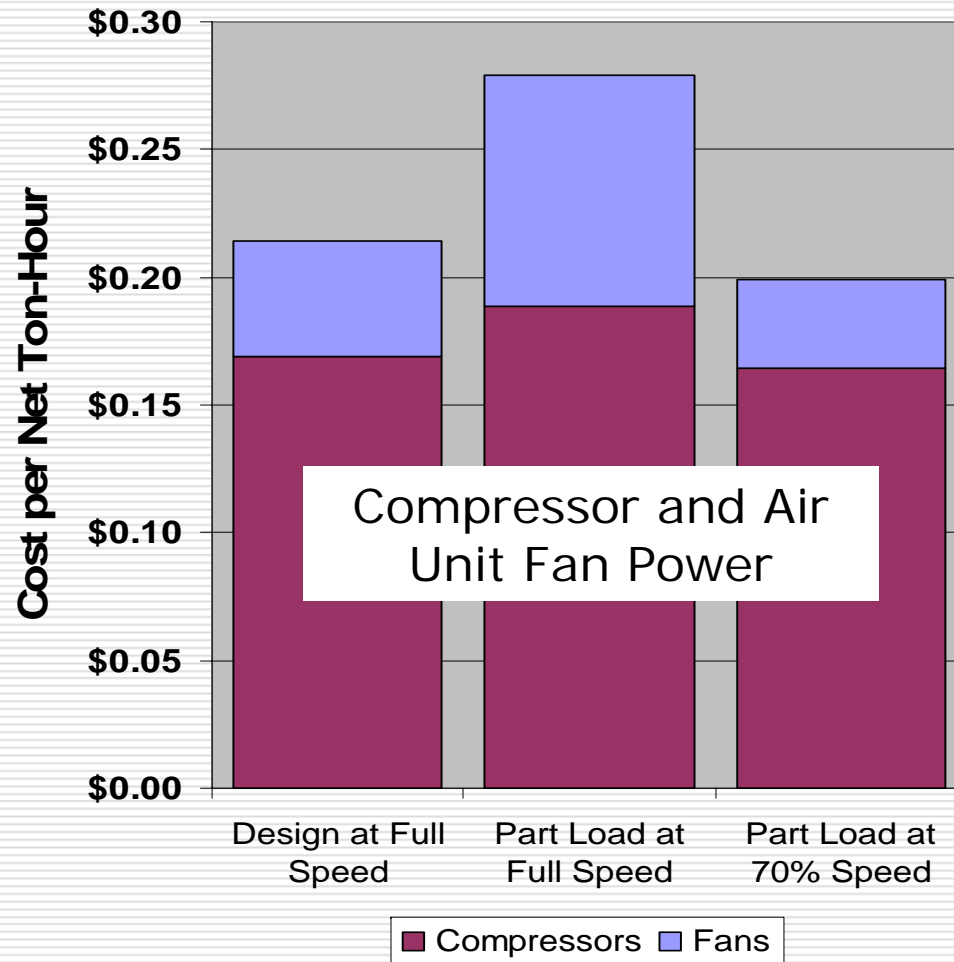
Fan power impact at average load

- ❑ Comparison of energy cost per ton-hour of net delivered cooling (before fan heat)
- ❑ Comparison:
 - Design values at 100% load and full speed fans
 - Average 50% cooling load with full speed fans
 - Average 50% cooling load with 70% fan speed
- ❑ 50,000 SF freezer, 200 tons design capacity

Fan power impact at average load

		Design	Part Load (50%)	
		Full Speed	Full Speed	70% Speed
Air Flow Rate (CFM/Ton)		1,852	3,017	2,385
Fan Power (Watts/Ton)		359	652	281
Cost (\$/Ton-Hour)	Fan	\$ 0.040	\$ 0.080	\$ 0.031
	Compressor	\$ 0.167	\$ 0.184	\$ 0.163
	Total	\$ 0.207	\$ 0.264	\$ 0.194
% Change from Design			28%	-7%
% Change from Part Load, Full Speed to Variable Speed				-27%
Annual Energy (KWh)	Fan		700,800	267,522
	Compressor		1,612,979	1,428,131
	Total		2,313,779	1,695,653
Annual Energy Cost (at \$.10/kWh)		-	\$ 231,378	\$ 169,565
Annual Savings				\$ 61,813
Savings per Cu. Ft.				\$ 0.04

Fan power impact at average load



Case study – small distribution

- ❑ Cold storage warehouse in Ontario, California with 20,000 SF of cooler and freezer

Energy Savings, kWh	280,000
Annual Cost Savings	\$27,600
Measure Cost	\$65,000
Incentive	<u>\$22,500</u>
Net Cost	\$42,500

- ❑ Hourly simulation

Payback, Years **1.5**

- ❑ Base case = fixed fan speed

IRR **68%**

- ❑ Savings based on variable speed with 70% minimum speed

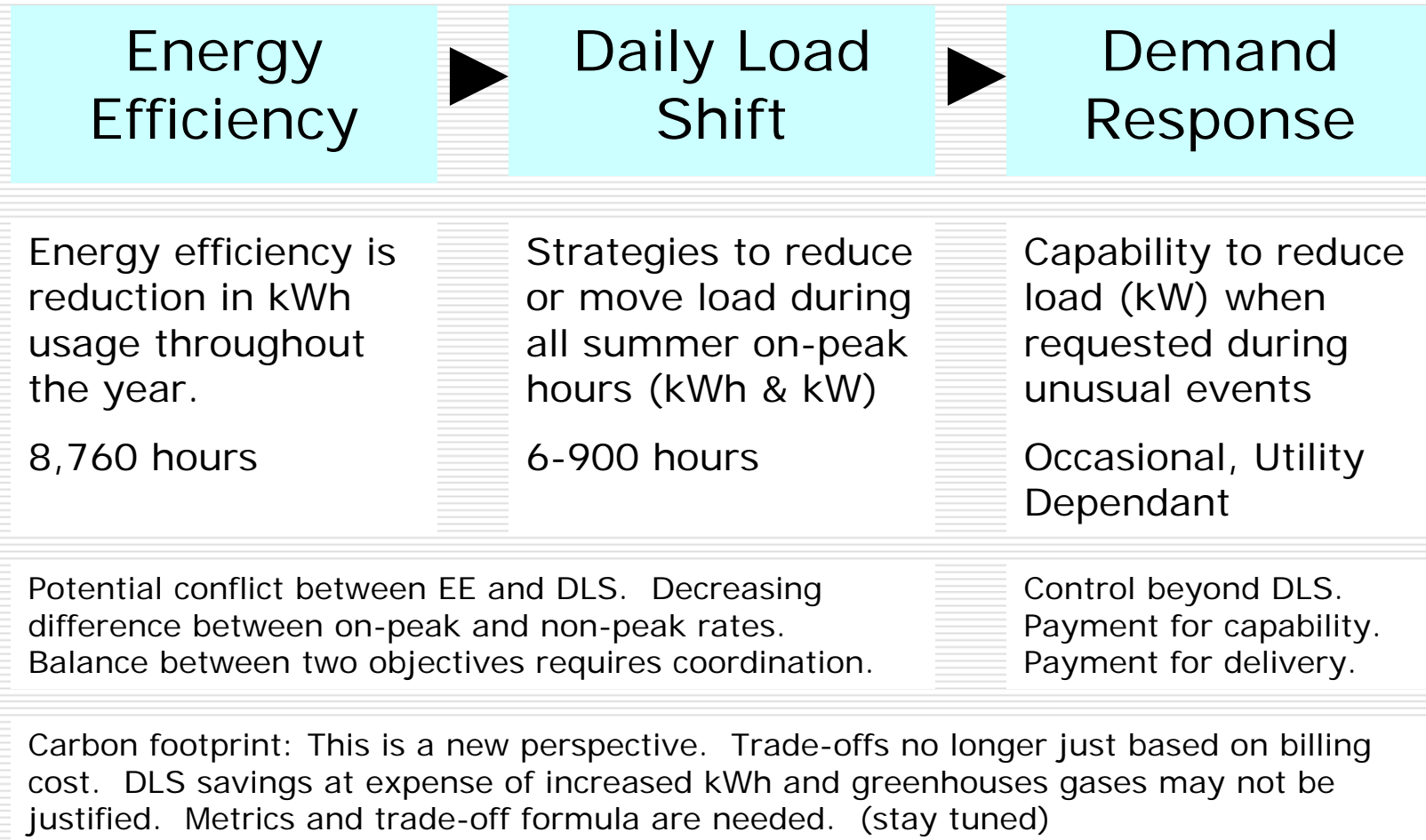
NPV **\$205,000**

Concerns and challenges

- ❑ Will air fall on the floor (not enough throw)?
 - Airflow reduction reduces terminal velocity not throw
- ❑ Will motors burn out?
 - Use proper motors, wiring practice, filters if needed
 - Don't (need to) run too slow
- ❑ Coils won't feed, won't defrost, etc.
 - Don't run too slow (diminishing returns)
 - Design and control anticipating variable volume
- ❑ Structure, racking and product obstructions
 - Issue of quantity of air vs. quality of distribution
 - Improve airflow quality: cost/benefit question

Energy Efficiency vs. Demand Management

Efficiency and demand hierarchy



Refrigeration & demand control

- Thermal mass
 - Refrigerated warehouses – inherent thermal storage in refrigerated product mass, cool during off-peak
- Variable speed changes the picture
 - Amount of cooling delivery can be modulated; essential to avoid 100% fan power
 - (May not be optimum to simply shut-off during on-peak and then overcool during non-peak)
- Scheduled cooling vs. setpoint control
 - Develop predictive load control (ton-hour delivery)
 - Optimize cost and resource use by delivery daily cooling in most effective manner

Maintenance and Energy Efficiency

Maintenance considerations

- ❑ How can refrigeration efficiency be optimized on a day-to-day basis?
- ❑ Compare operations with expectations:
 - Ambient + TD = expected SCT
 - Box temp – TD = expected SST
 - Use saturation temperatures not pressures
- ❑ Know the “sweet spots” (e.g. 60-80% speed)

- ❑ Proactive effort vs. tendency to wait until deficiency become a pressing need or “its number comes up”

Efficiency faults

- ❑ Understand efficiency “faults” where system keeps working but energy use goes up
- ❑ Low refrigerant charge – how big is this?
 - Low charge equivalent to hot-gas bypass
 - Applies to DX systems AND industrial systems
- ❑ Refrigerant integrity
 - Moisture, non-condensables, oil (in wrong place)
 - Results in heat exchanger TD above expectations

Performance Monitoring

Performance monitoring

- Remote efficiency monitoring
 - Real time, continuous performance analysis
 - Web based results presentation (wider audience)
- Rationale
 - Management by exception, must measure to manage
 - Refrigeration systems don't come with efficiency "meters"; designed to always meet load
- Performance measures
 - Energy efficiency metrics: kW/Ton, \$/Ton-Hr
 - Maintenance and performance indicators
 - Key trends (e.g. refig. level, inventory)

Total System

Energy Rates

Energy Consumption

Power Graphs

Reports

System Information

Data

Compressors-1

Compressors-2

Suction Group

Heat Rejection

Zones - Temperature

Zones - Fan Cycle

Refrigeration Monitoring System - Demo Site

Select Time Period to View Data and Click on 'Process Data' Button

Start Time/Date

April 2007

Sun	Mon	Tue	Wed	Thu	Fri	Sat
25	26	27	28	29	30	31
1	2	3	4	5	6	7
8	9	10	11	12	13	14
15	16	17	18	19	20	21
22	23	24	25	26	27	28
29	30	1	2	3	4	5

Today: 5/1/2007

12:00:00 AM

End Time/Date

April 2007

Sun	Mon	Tue	Wed	Thu	Fri	Sat
25	26	27	28	29	30	31
1	2	3	4	5	6	7
8	9	10	11	12	13	14
15	16	17	18	19	20	21
22	23	24	25	26	27	28
29	30	1	2	3	4	5

Today: 5/1/2007

12:00:00 AM

Time Filter

- Sel. Period
- 5 Minutes
- 15 Minutes
- Hourly
- Daily
- Weekly
- Monthly

Data Processing Results

Selected Time Period: 4/2/2007 TO: 4/4/2007

Selected Time (Hr): 48.000

Data Processing Progress: 

Collected Data (Hr): 48.000

Processed Data Start Date/Time: 9/29/2004

Data Collection Rate (%): 100.000

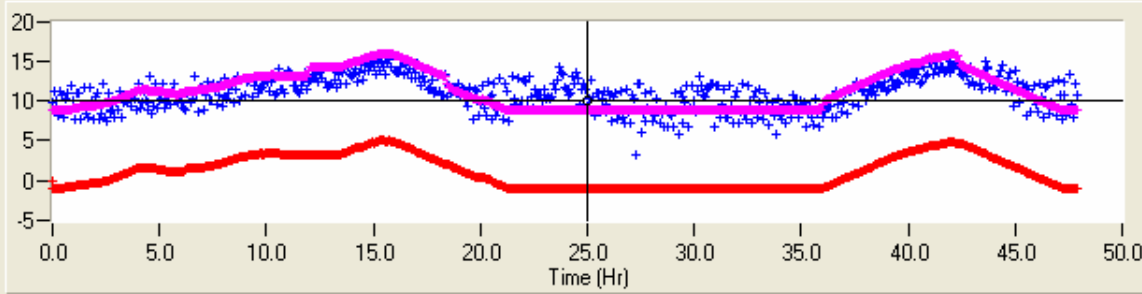
Processed Data End Date/Time: 5/1/2007 10:00:00 AM

Status: Data Retrieved and Processed

Process Data

Suction Group: LT

Suction Pressure - Current (PSIG), Target (PSIG), Float



Graph Mode
 Cursor Mode
 Zoom Mode

Cursor: Time/Data

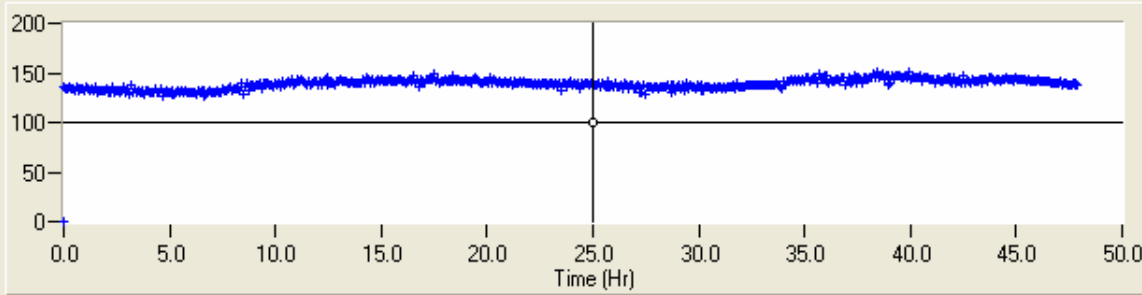
Design SST: -10 °F
Design SCT: 90 °F

Suction Pressure Current (PSIG): *

 Suction Pressure Target (PSIG): *

 Suction Pressure Float: *

Discharge Pressure (PSIG)

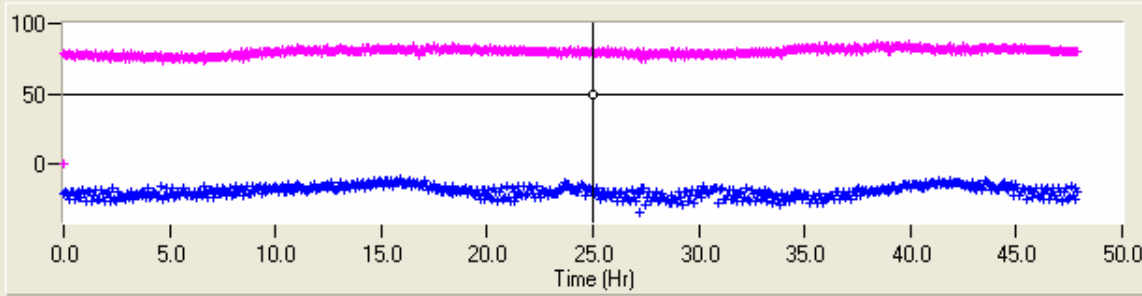


Graph Mode
 Cursor Mode
 Zoom Mode

Cursor: Time/Data

Discharge Pressure (PSIG): *

SST (DegF) and SDT (DegF)



Graph Mode
 Cursor Mode
 Zoom Mode

Cursor: Time/Data

SST (DegF): *

 SCT (DegF): *

 kW/Ton *

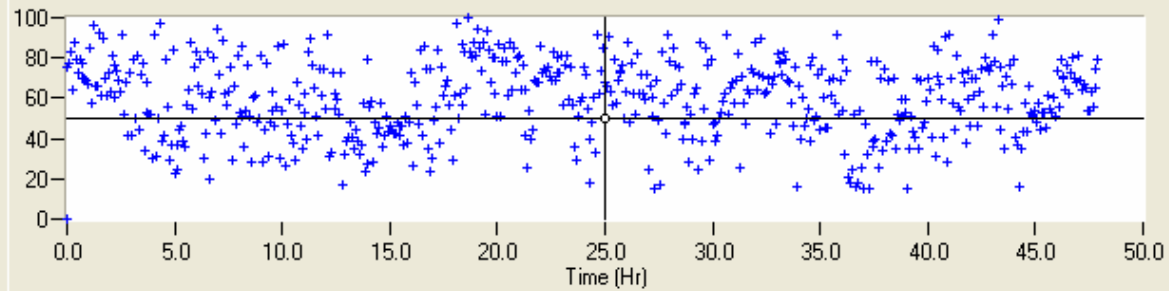
 Power (kW): *

 Refrigeration (Tons) *

* Period Average

Condenser: Low Temp EC2

Condenser VFD Speed Set Point (%)

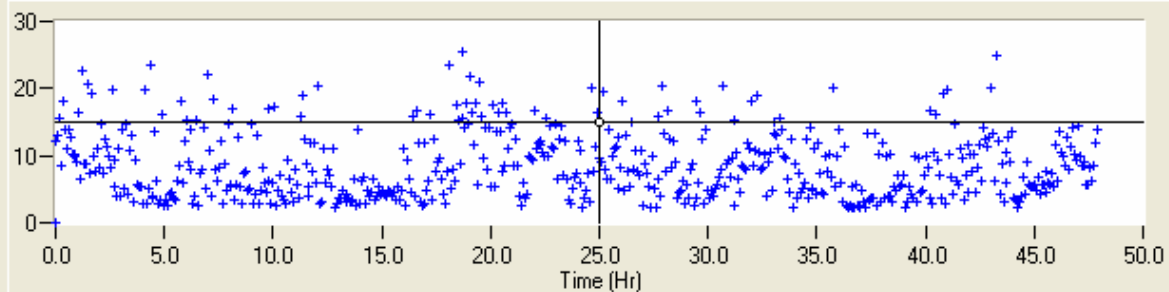


Graph Mode
 Cursor Mode
 Zoom Mode

Cursor: Time/Data

Fan Speed (%): *
59.5

Condenser Power (kW)

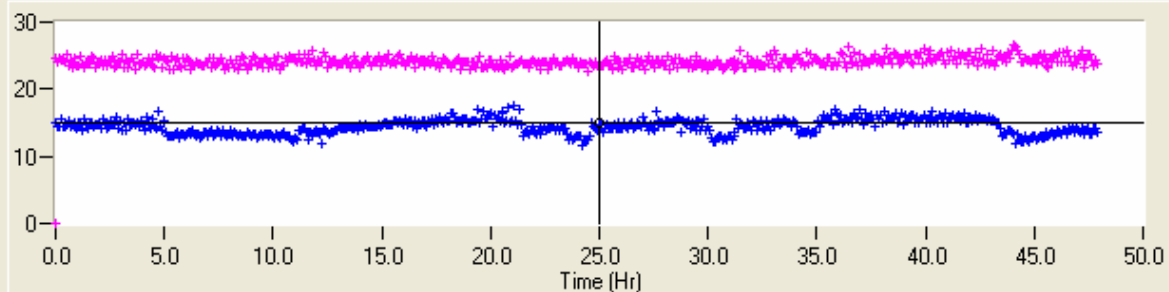


Graph Mode
 Cursor Mode
 Zoom Mode

Cursor: Time/Data

Condenser Power (kW): *
7.1

High Pressure Receiver Levels



Graph Mode
 Cursor Mode
 Zoom Mode

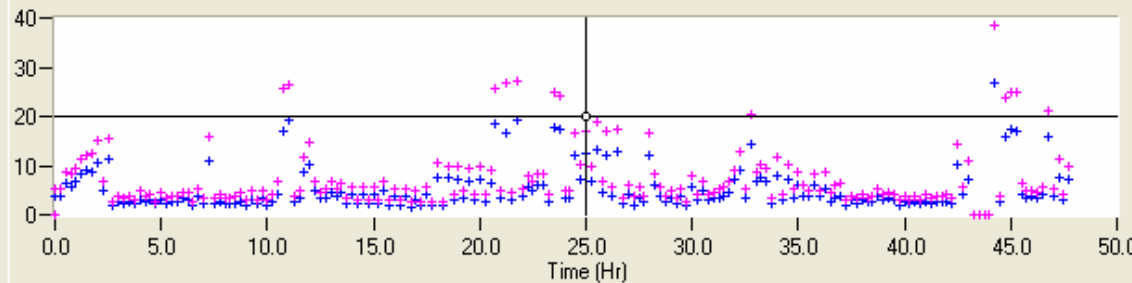
Cursor: Time/Data

EC1 HP Receiver Level (%): *
14.4

EC2 HP Receiver Level (%): *
24.1

* Period Average

Refrigeration System kW/Ton - With Calculated Power and With Measured Power



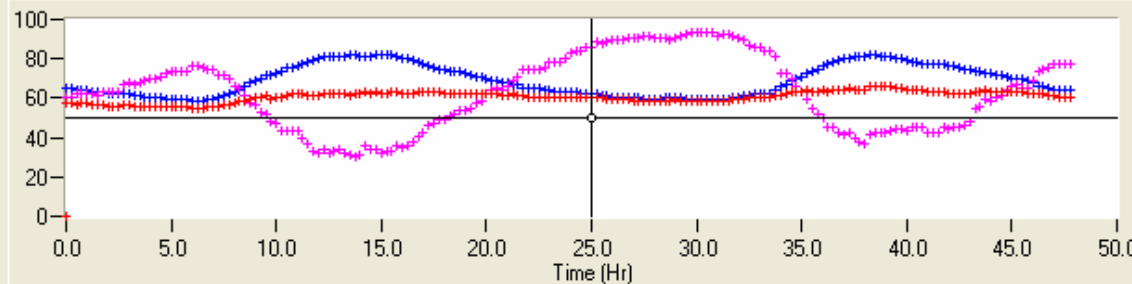
Graph Mode
 Cursor Mode
 Zoom Mode

Cursor: Time/Data

kW/Ton *
 (Excluding Air Units)

 kW/Ton *:
 (Including Air Units)

Ambient Parameters - DBT (DegF), RH (%), WBT (DegF)



Graph Mode
 Cursor Mode
 Zoom Mode

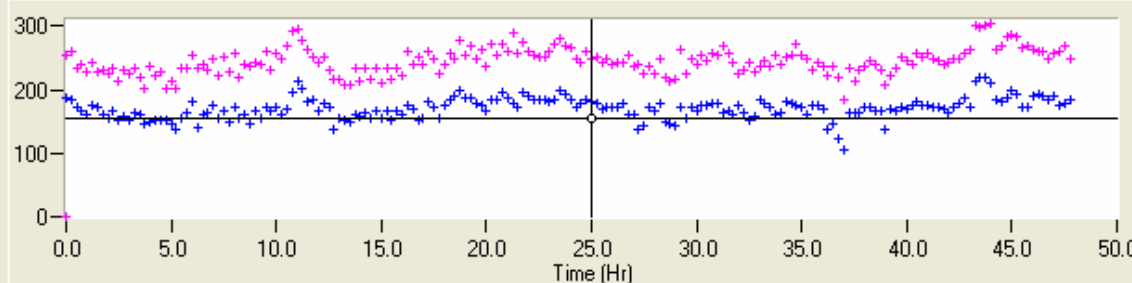
Cursor: Time/Data

Ambient DBT (DegF) *

 Ambient RH (%) *

 Ambient WBT (DegF) *

Refr. System Power - Calculated Power (kW) Measured Power (kW)



Graph Mode
 Cursor Mode
 Zoom Mode

Cursor: Time/Data

Refr System Power (kW) *
 (Excluding Air Units)

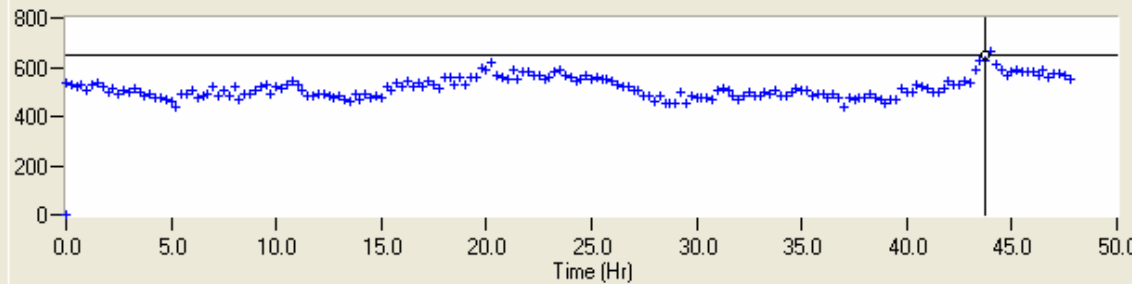
 Refr. System Power (kW) *
 (Including Air Units)

 Refr. System Energy (kWh)
 (Excluding Air Units)

 Refr System Energy (kWh)
 (Including Air Units)
 * Period Average

Power System: Total

Demand (kW)



Graph Mode
 Cursor Mode
 Zoom Mode

Cursor: Time/Data
 04/03/07 19:13:00
 649.06

Demand (kW): *

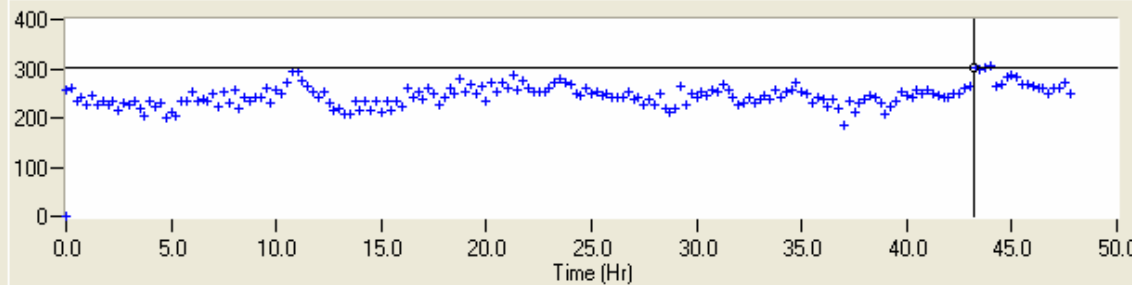
516.9

Energy (kWh):

24809.7

Power System: Refr

Demand (kW)



Graph Mode
 Cursor Mode
 Zoom Mode

Cursor: Time/Data
 04/03/07 19:13:00
 301.89

Demand (kW): *

245.3

Energy (kWh)

11775.3

* Period Average

Performance monitoring

Going forward

- ❑ Essential to achieve continued gains in energy efficiency and meet global environmental needs
- ❑ Global interest and attention (e.g. ASHRAE)
- ❑ Means to bring experts closer to needs
- ❑ Build into control systems (push down)
- ❑ Help connect end-to-end expectations
 - Do systems run per design?
 - Is equipment sized right?
 - Feedback to vendors, engineers and maintenance
- ❑ Bottom line: maximize life-cycle value

Questions?